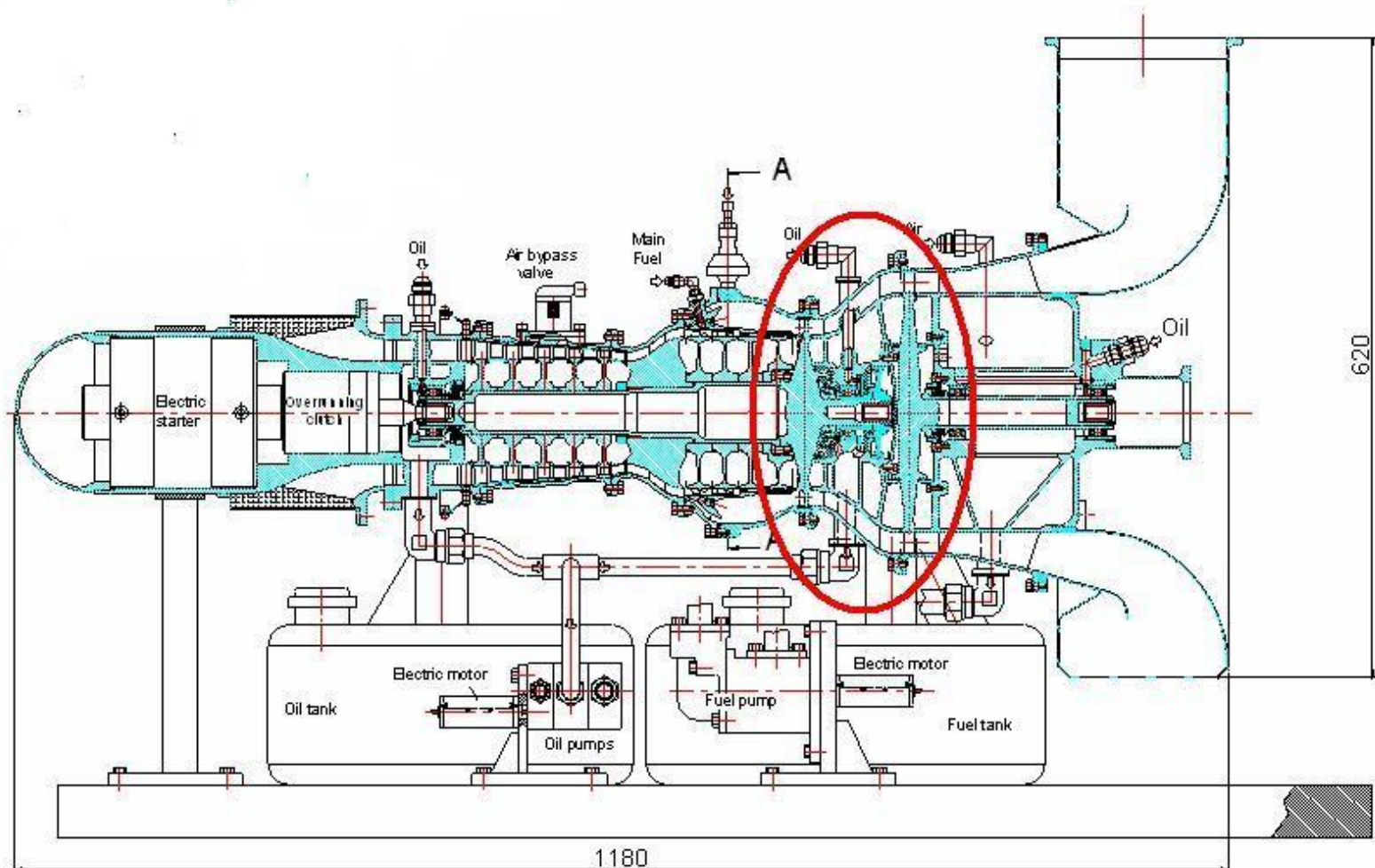


# **Swirling Flow in Annular Diffusers Between Two Counter-Rotating Turbines**

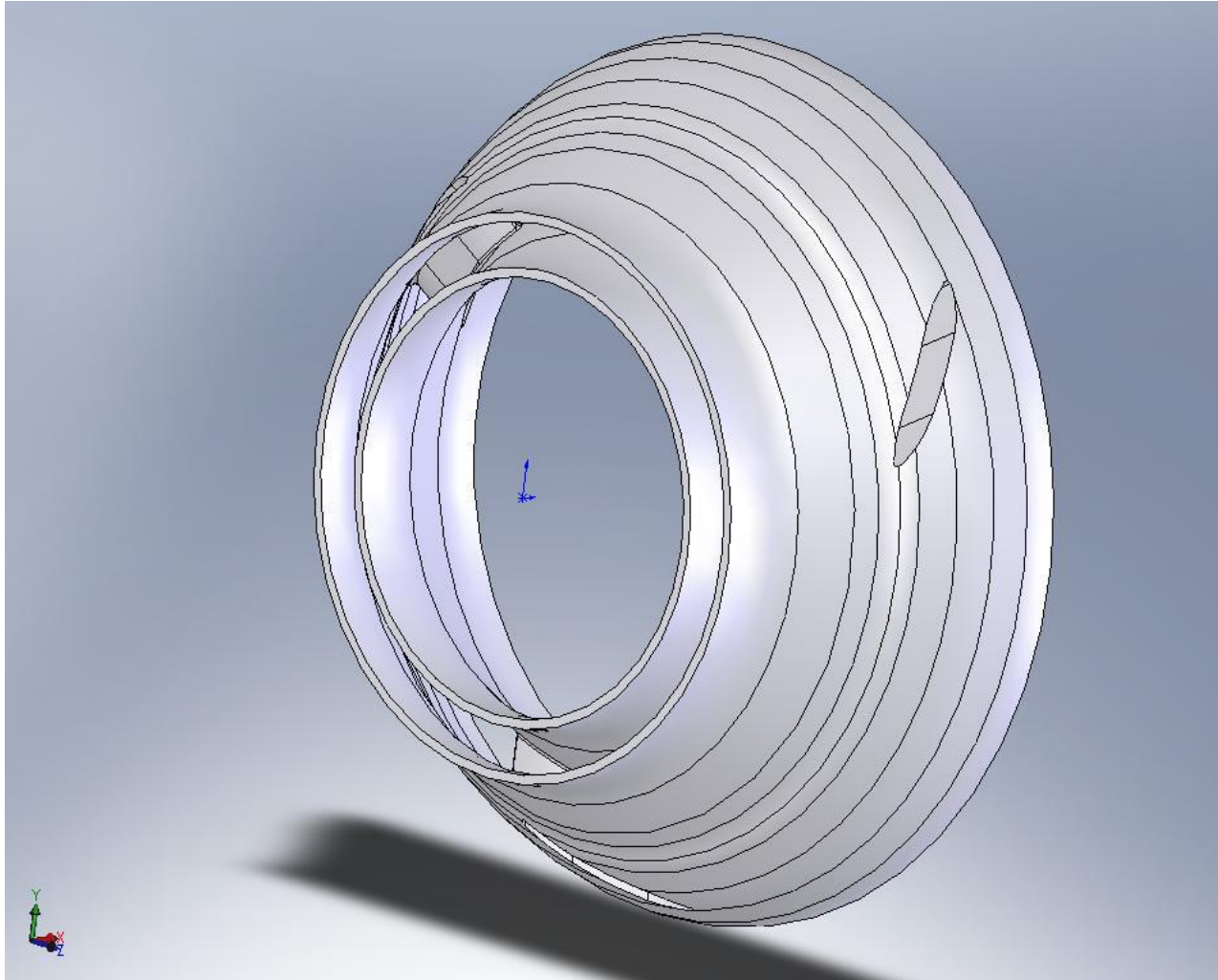
**Prepared by: Dr. Vladimir Erenburg**

# Swirling Flow in Annular Diffuser



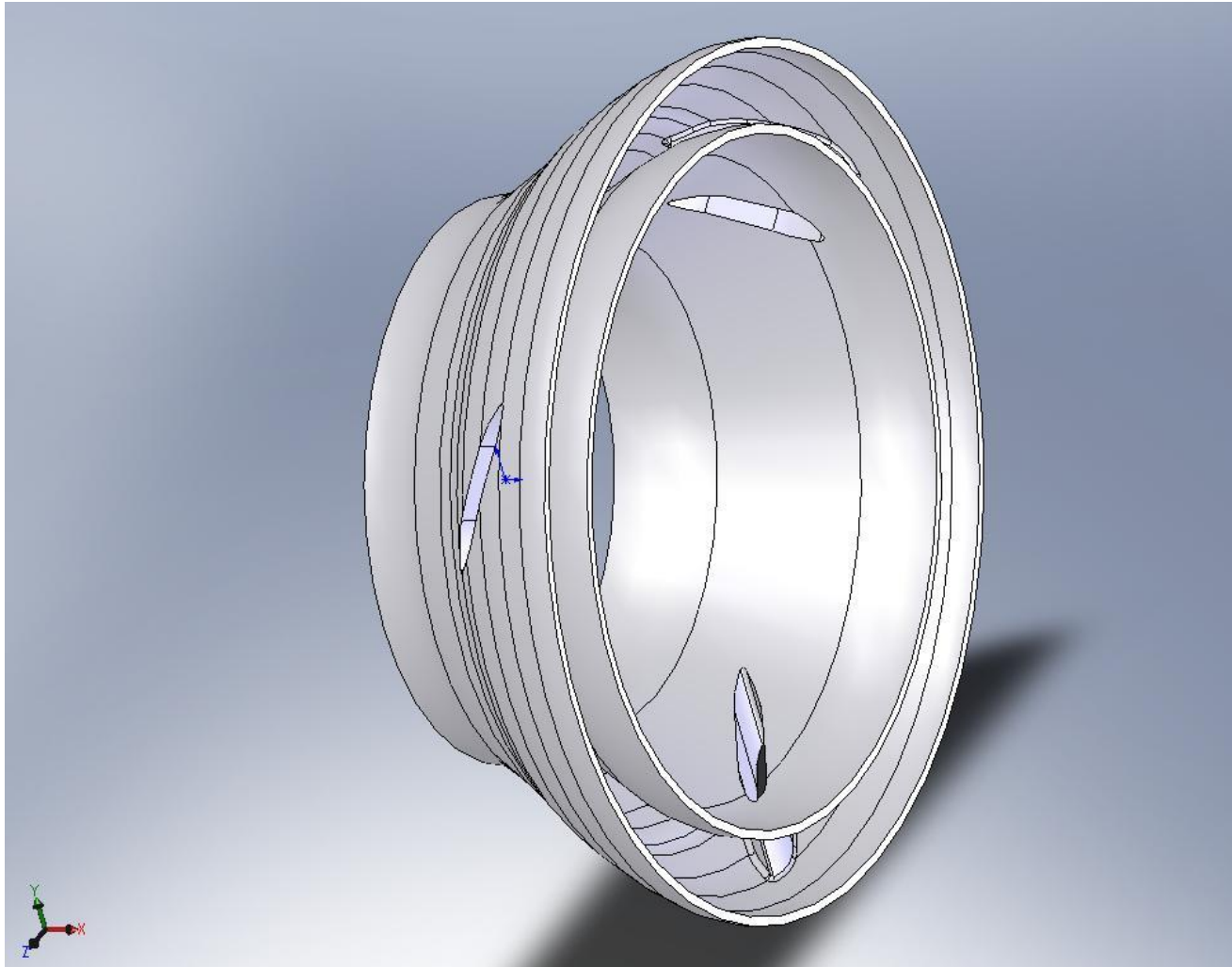
# Swirling Flow in Annular Diffuser

## CAD Model



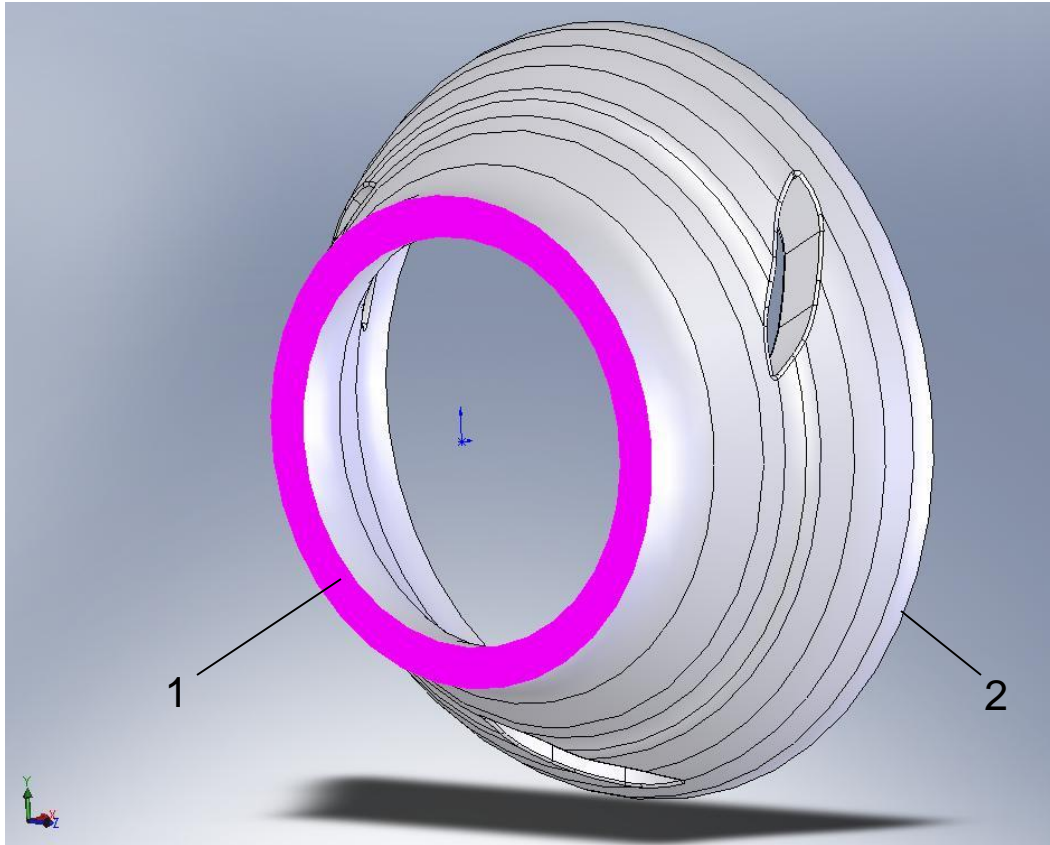
# Swirling Flow in Annular Diffuser

## CAD Model



# Swirling Flow in Annular Diffuser

## Calculated Domain and Boundary Conditions



### Mass-Flow Inlet:

$$Q=1.528 \text{ kg/s}$$

$$\alpha=58.8^\circ$$

$$T_0=1202K$$

### Outlet-Vent:

$$p_s=\text{const},$$

$$\zeta=\text{const},$$

$$\zeta=\Delta p/(\rho v^2/2) - \text{loss coefficient}$$

Figure 1. 1 – mass flow inlet, 2 – outlet-vent

# Swirling Flow in Annular Diffuser

## Governing Equations

$$\frac{\partial u_i}{\partial t} + \frac{\partial}{\partial x_j} (u_i u_j) = -\frac{1}{\rho} \frac{\partial p}{\partial x_i} + \frac{\partial}{\partial x_j} \left( \nu \left( \frac{\partial u_i}{\partial x_j} - \frac{2}{3} \frac{\partial u_i}{\partial x_i} \right) - \mu \bar{u}_i' \bar{u}_j' \right) \quad (1)$$

$$\frac{\partial \rho}{\partial t} + \frac{\partial (\rho u_i)}{\partial x_i} = 0 \quad (2)$$

$$\rho \frac{di}{dt} = A \frac{dp}{dt} + \frac{\partial}{\partial x_i} \lambda \frac{\partial T}{\partial x_i} \quad (3)$$

## The Models of Turbulence

### ***k-ε models:***

Realizable

RNG-based

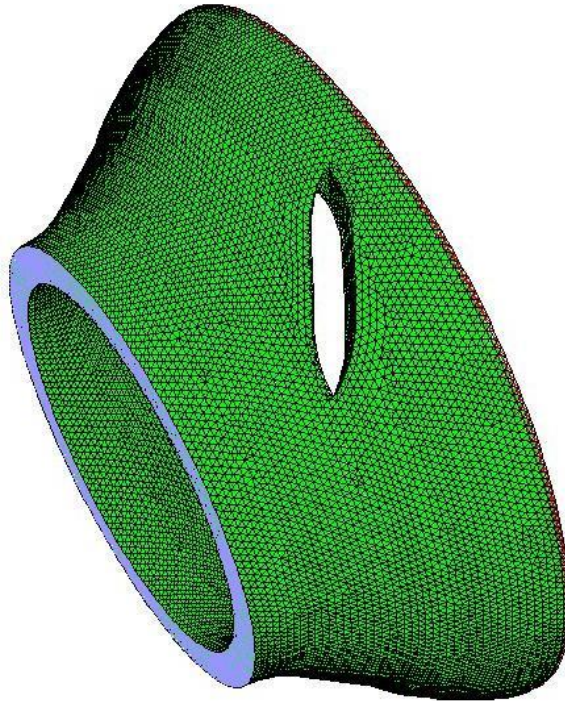
### ***k-ω standard model***

### ***Reynolds Stress Model (RSM)***

**FLUENT , GAMBIT**

# Swirling Flow in Annular Diffuser

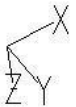
## Calculated Grid



Unstructured Tetrahedral Grid

Base grid: ~350,000 cells

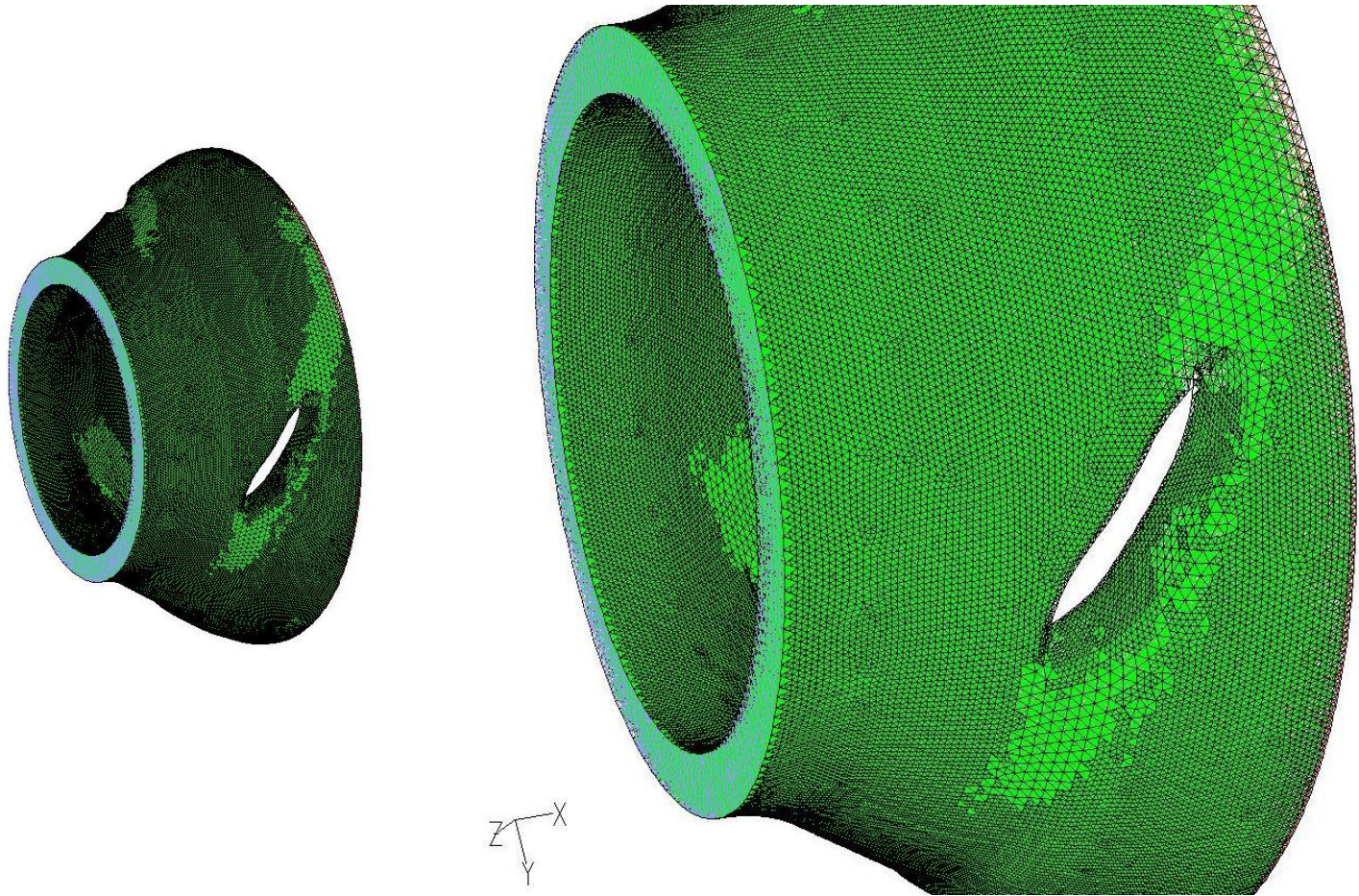
Adapted grid: ~600,000 cells





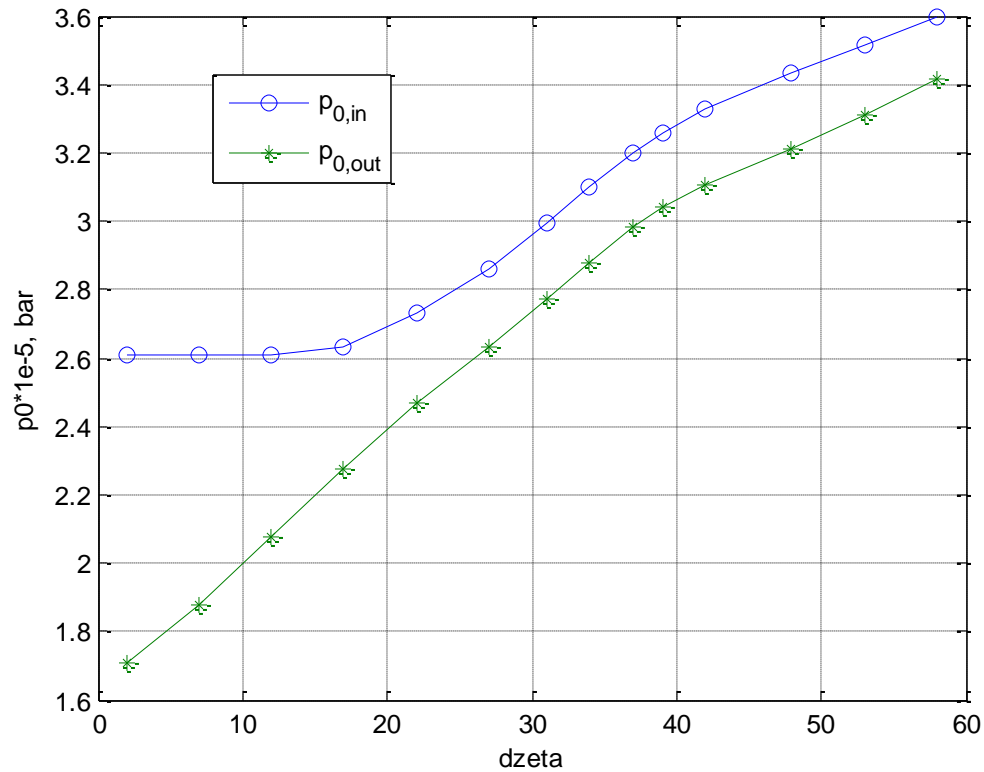
# Swirling Flow in Annular Diffuser

## Gradient Adaptation



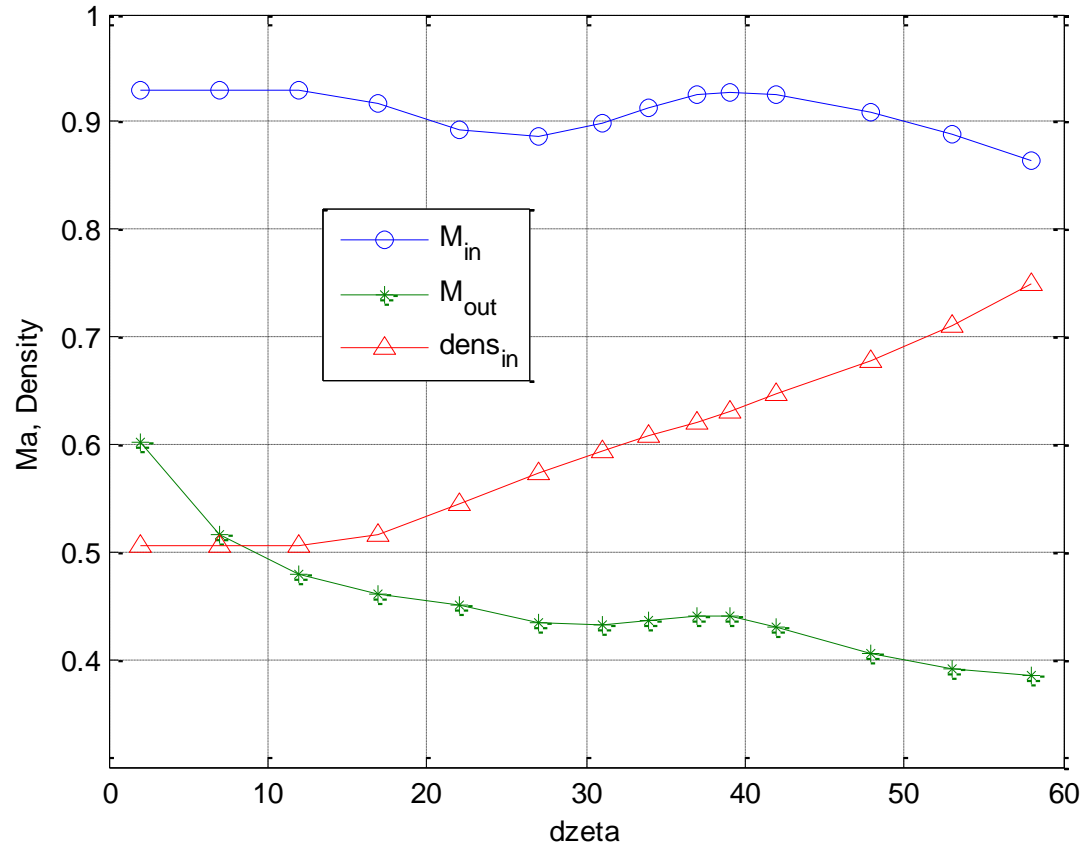


# Swirling Flow in Annular Diffuser



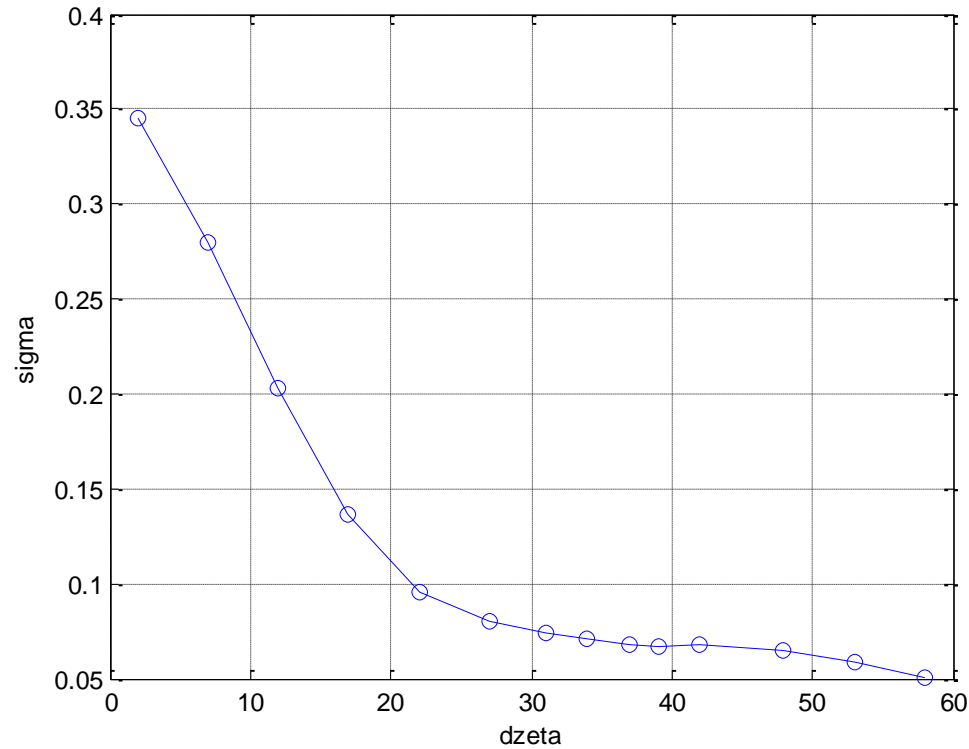
**Figure 2.** Total pressure at inlet and outlet sections

# Swirling Flow in Annular Diffuser



**Figure 3.** Mach number and density as functions of  $\zeta$

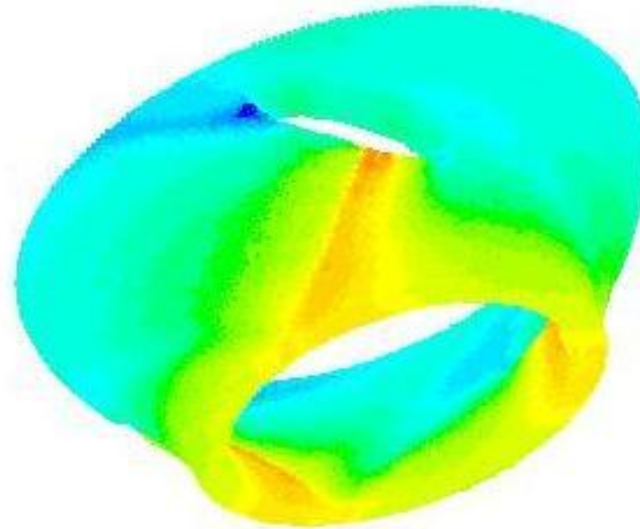
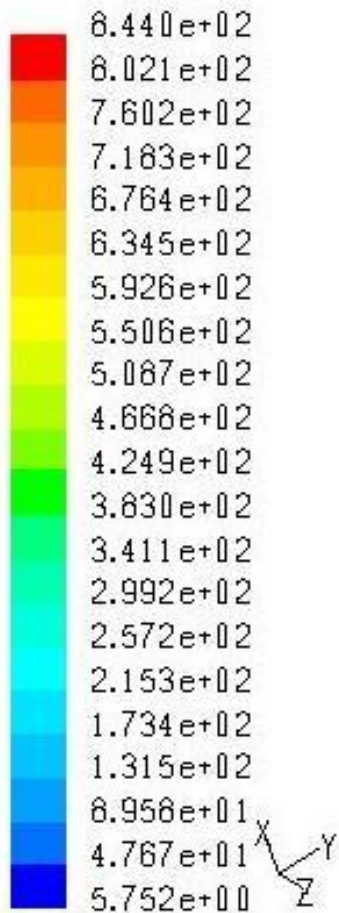
# Swirling Flow in Annular Diffuser



$$\sigma = \frac{p_{0,in} - p_{0,out}}{p_{0,in}}$$

**Figure 4.** Total pressure losses

# Swirling Flow in Annular Diffuser

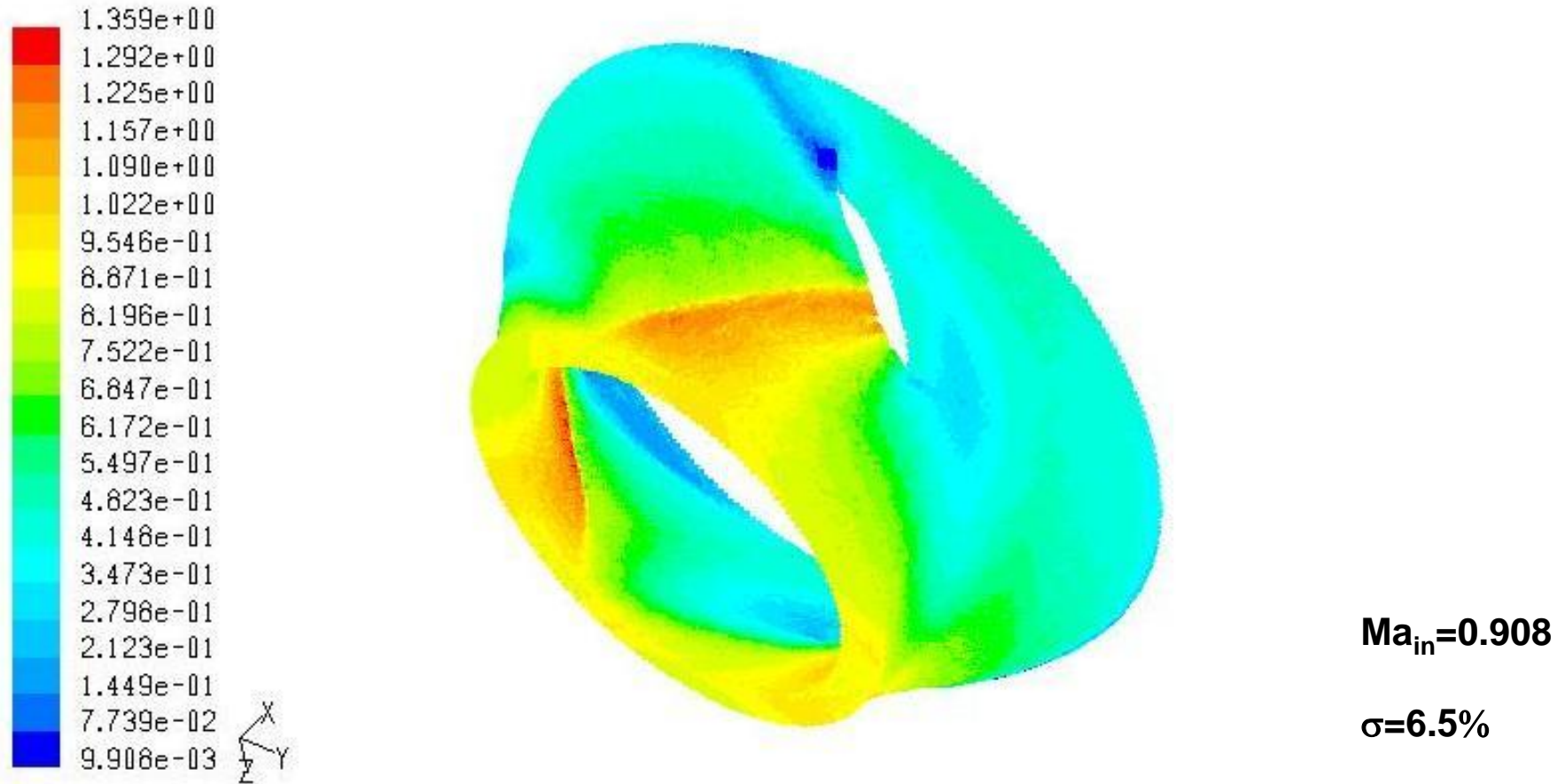


$Ma_{in}=0.864$

$\sigma=5.1\%$

**Figure 5.** Velocity Magnitude,  $\zeta=58$

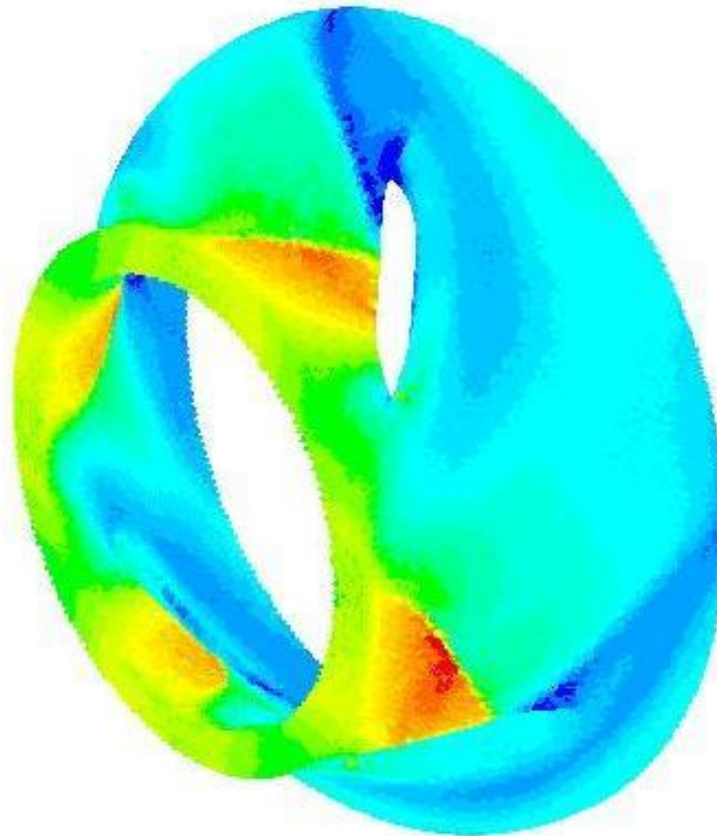
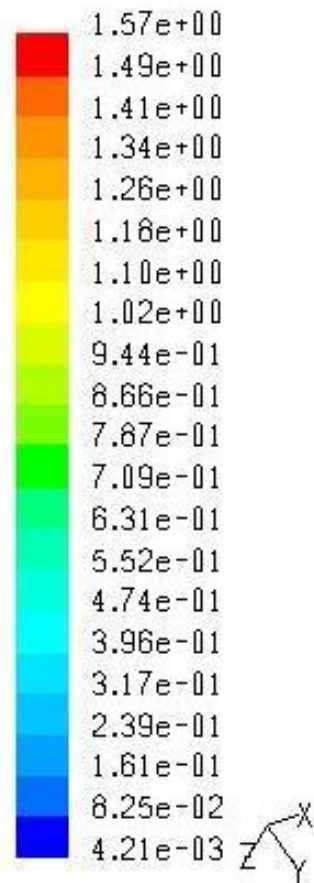
# Swirling Flow in Annular Diffuser



**Figure 6.** Mach number,  $\zeta=47.9$



# Swirling Flow in Annular Diffuser

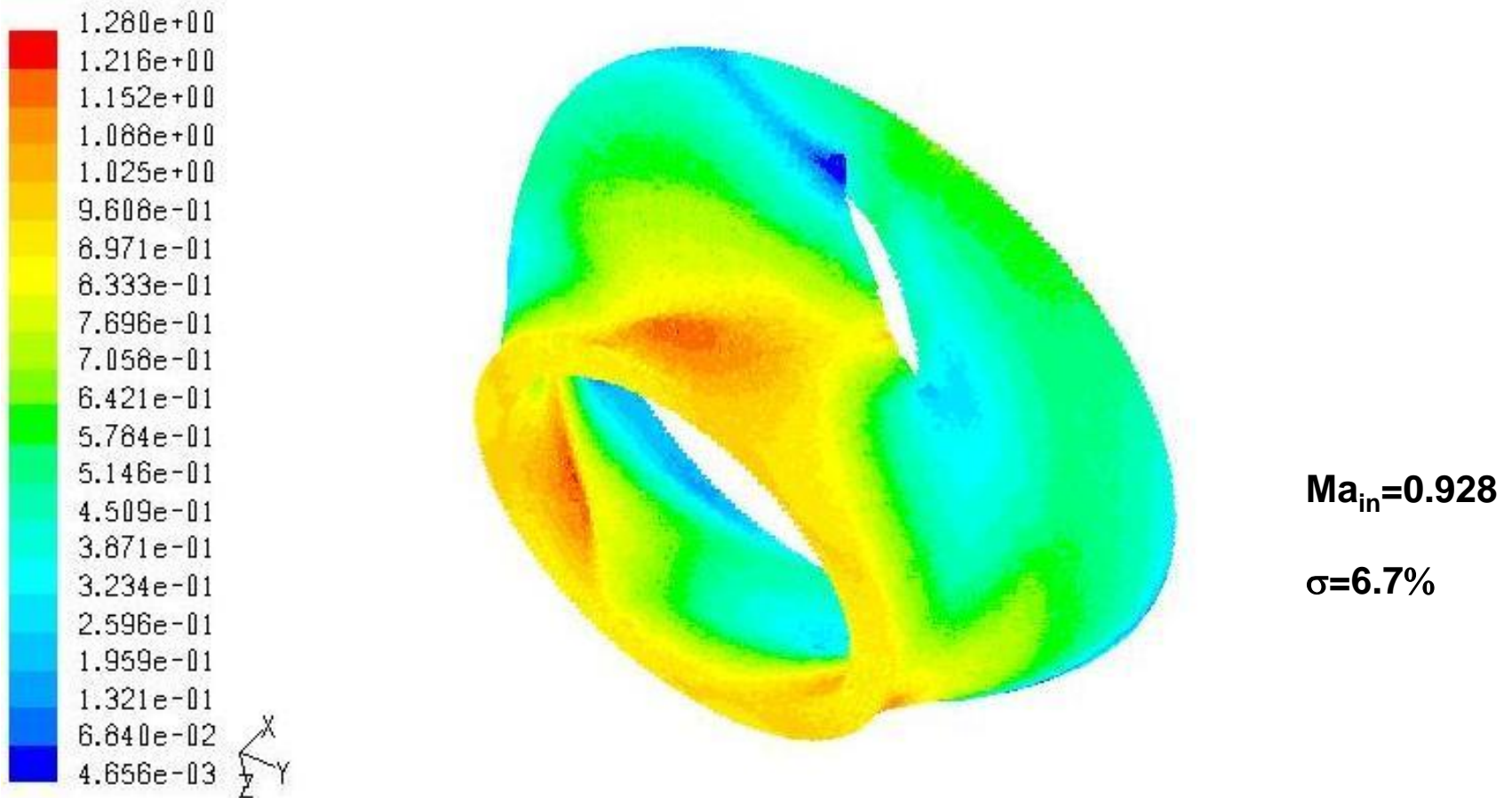


$Ma_{in}=0.870$

$\sigma=9.8\%$

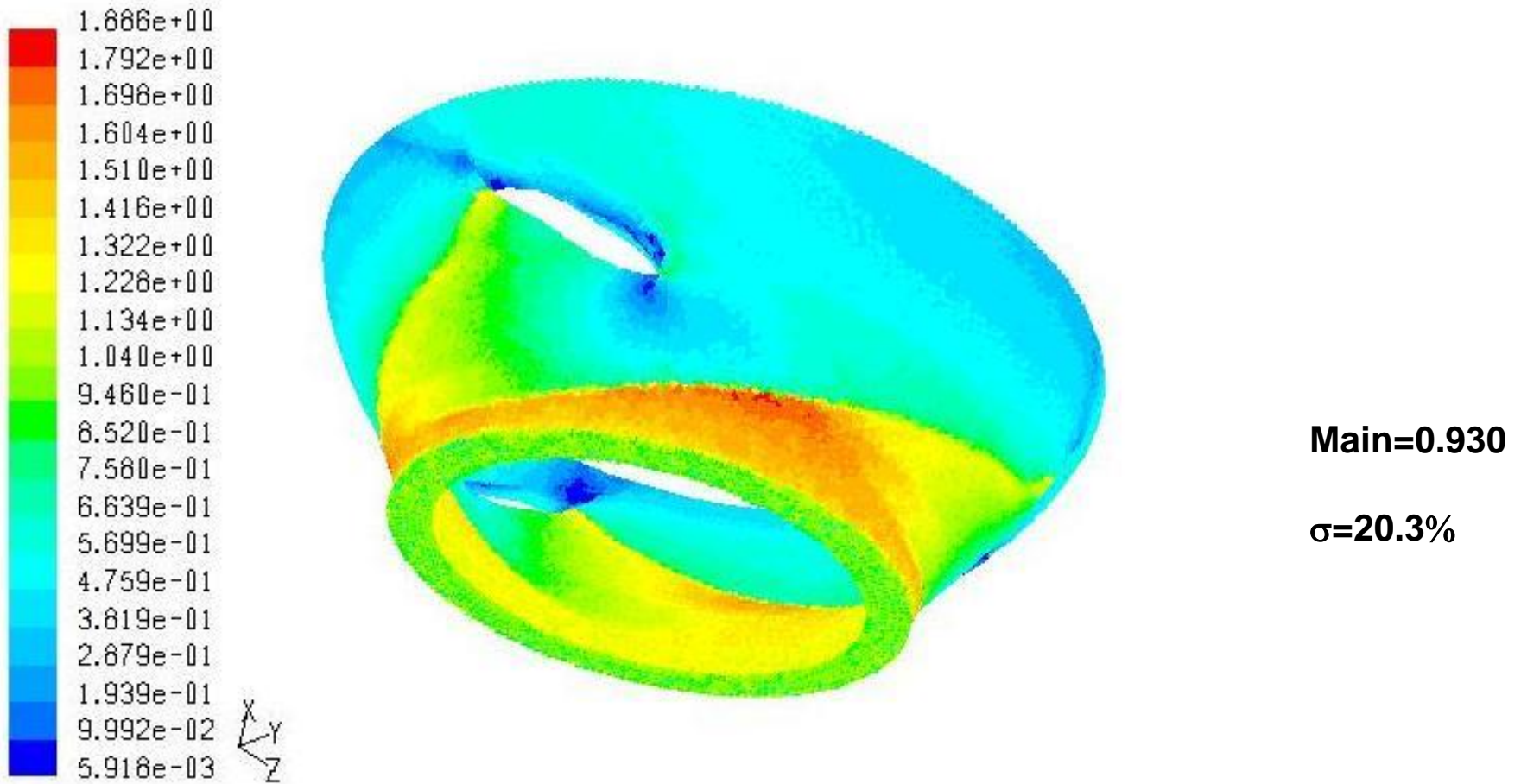
**Figure 7.** Mach number in non-optimal diffuser,  $\zeta=47.9$

# Swirling Flow in Annular Diffuser



**Figure 8.** Mach number ,  $\zeta=39$

# Swirling Flow in Annular Diffuser



**Figure 9.** Mach number ,  $\zeta=12$

# Swirling Flow in Annular Diffuser

## Effects of the Models of Turbulence

Table 1. Comparison for different models,  $\zeta=47.9$

Model	$p_{0,in}$ , bar	$p_{0,out}$ , bar	$Ma_{in}$	$Ma_{out}$	$ v _{,in}$ , m/s	$\sigma$ , %
Realizable	3.436	3.212	0.908	0.405	568.5	6.52
RNG	3.435	3.221	0.907	0.410	567.8	6.23
k- $\omega$	3.490	3.216	0.916	0.410	579.1	7.85
RSM	3.434	3.223	0.907	0.413	572.6	6.14

## Effect of Grid Adaption

Table 2. k- $\varepsilon$  Realizable Model,  $\zeta=47.9$

Grid	$p_{0,in}$ , bar	$p_{0,out}$ , bar	$Ma_{in}$	$Ma_{out}$	$ v _{,in}$ , m/s	$\sigma$ , %
Base	3.436	3.212	0.908	0.405	568.5	6.52
Adapted	3.444	3.214	0.908	0.410	574.5	6.68

Adapted grid,  $p_{0,in}=3.3$  bar  $\Rightarrow$   **$6.5\% \leq \sigma \leq 7.7\%$**

# Swirling Flow in Annular Diffuser

## CONCLUSIONS

1. It is possible on the base of CFD modeling to optimize configuration of intermediate diffuser to reduce to a minimum pressure losses owing to correct choice of its profile, and number, location and direction of vanes.
2. Failing experimental data we can't prefer either of considered models of turbulence. Therefore on the base of carried study we suppose that calculated total pressure losses are in the limits from 6.5% to 7.7%